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Article

Development of Molecular Distillation Based Simulation and Optimization of Refined Palm Oil Process Based on Response Surface Methodology

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Abstract: The deodorization of the refined palm oil process is simulated here using ASPEN HYSYS. In the absence of a library molecular distillation (MD) process in ASPEN HYSYS, first, a single flash vessel is considered to represent a falling film MD process which is simulated for a binary system taken from the literature and the model predictions are compared with the published work based on ASPEN PLUS and DISMOL. Second, the developed MD process is extended to simulate the deodorization process. Parameter estimation technique is used to estimate the Antoine's parameters based on literature data to calculate the pure component vapor pressure. The model predictions are then validated against the patented results of refining edible oil rich in natural carotenes and vitamin E and simulation results were found to be in good agreement, within a $\pm 2\%$ error of the patented results. Third, Response Surface Methodology (RSM) is employed to develop non-linear second-order polynomial equations based model for the deodorization process and the effects of various operating parameters on the performance of the process are studied. Finally, an optimization framework is developed to maximize the concentration of beta-carotene, tocopherol and free fatty acid while optimizing the feed flow rate, temperature and pressure subject to process constraints. The optimum results of feed flow rate, temperature, and pressure were determined as 1291 kg/h, 147 °C and 0.0007 kPa respectively, and the concentration responses of beta-carotene, tocopherol and free fatty acid were found to be 0.000575, 0.000937 and 0.999840 respectively.

Keywords: process simulation; ASPEN HYSYS; molecular distillation; response surface methodology; optimization

1. Introduction

Palm oil is consumed worldwide. It is known that edible palm oil is full of nutrients that contribute to daily energy needs. The general compositions of crude palm oil are 95% of triglycerides, 3%–5% of fatty acid and 1% of minor trace component (phytonutrient). Palm oil is rich in phytonutrients; it provides a valuable source of beta-carotene and tocopherol (vitamin E). Crude palm oil has carotenes concentration of 1000 ppm–3000 ppm [1]. The carotenes from palm oil are a source of pro-vitamin A and recent findings have demonstrated that beta-carotene is used to inhibit tumor progression and hence, reduces cancer formation in humans. The purpose of the refined palm oil process is to remove unwanted fatty acid and impurities. It can be classified as both chemical and physical refining method. However, the physical method is proven to be more effective compared to the chemical method in terms of food safety and environment [2]. The physical method consists of three processes; degumming, bleaching and deodorization. The pre-process of deodorization involves operation at a temperature higher than 200 °C at normal pressure. It is performed to remove odor from the oil and

additional fat. It generally results in not only removing fatty acid but also destroying all carotenes. Most of the carotenes in palm oil are destroyed in the conventional refining process to produce a lighter color oil [3].

The molecular distillation (MD) technique is a viable process to recover carotene from the palm oil and is suitable for such high a value-added product [4]. It is an important thermal separation technology. Typical application involves high boiling substances mainly of temperature-sensitive compounds. The compounds are distilled at a pressure range from 1 atmosphere to high vacuum [5]. At this pressure the evaporation temperature will fall during the short residence time, hence, no thermal decomposition can occur. Due to pressure being low as vacuum sometimes, it is known as a vacuum distillation column. Mean free path has an effect on this separation process. The mean free path of MD column is longer than the distance of evaporator and condenser. As a result, the molecules reach the condensing surface without being swerved on collision of others foreign gas. The larger molecule size has a shorter mean free path. Therefore, MD separates substances by its molecular weight. The main objectives of this research are divided into four sections: (a) MD process development and validation for a binary system from literature; (b) Application of the MD process for palm oil deodorization and validation of the process against patented experimental data; (c) Design of experiment by Response Surface Methodology (RSM) leading to the development of non-linear equations based MD model for palm oil deodorization; and (d) Optimization of the deodorization process based on the non-linear equations developed in (c). Note, there are many prevalent applications of RSM in food science, chemical and biological engineering related to molecular distillation [6–9].

Optimization in engineering shows an important methodology to enhance the process rather than making decisions intuitively. Many techniques and algorithms, such as neural network, genetic algorithm, Monte Carlo, Excel solver and others have been successfully applied in various processes. Here, Excel solver has been used for optimizing the operation of the refined palm oil process. The simulation, design of experiment and optimization are presented and discussed in later sections.

2. Molecular Distillation Process: Modeling and Validation

In this work, MD is used for the deodorization of palm oil. The objective of this section is to develop and simulate a molecular distillation process. Since there was no library model available in ASPEN HYSYS to simulate a falling film molecular distillation therefore, a simulation of single flash vessel was proposed to represent MD, as considered by other authors in previous studies [10]. In order to ensure that the simulation of MD in ASPEN HYSYS was valid, we referred to the study by the authors of [10] for the development of a computational tool for simulating MD process in oil refining using ASPEN PLUS and validation of the results against those predicted by DISMOL (a dedicated molecular distillation process simulator). In their study, an equi-molar mixture of Dibutyl phthalate (DBP) and Dibutyl sebacate (DBS) was fed to the flash process at pressure 0.133 Pa with an initial feed flow rate of 50 kg/h. Temperature was manipulated to achieve the same distillation mass ratio with DISMOL simulator (0.2120). Their ASPEN PLUS results are shown in Figures 1 and 2 together with the results of this work, which used ASPEN HYSYS with Redlich Kwong Soave with Wong Sandler mixture rules (RKSWS) for the calculation of thermo-physical properties.

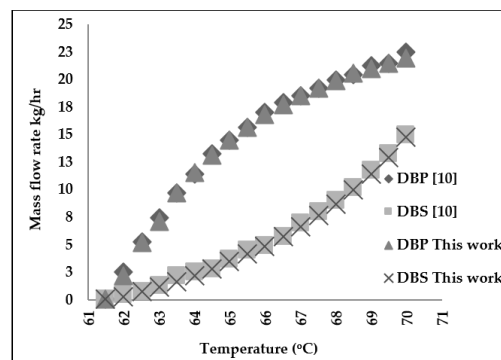


Figure 1. Comparison of distilled mass flow rate in study [10] and this work as a function of flash vessel operating temperature (°C).

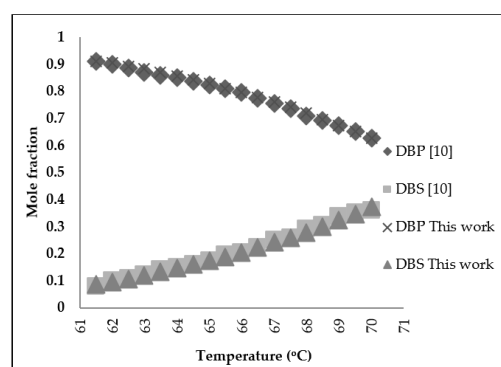


Figure 2. Comparison of distillate mole fraction in study [10] and this work as a function of flash vessel operating temperature (°C).

The plotted data between ASPEN PLUS and ASPEN HYSYS seem to be in very good agreement. In order to achieve the same distillation mass ratio obtained by DISMOL, the flash equipment for ASPEN PLUS and ASPEN HYSYS had to operate at a temperature of 63.1 °C and 63.5 °C respectively. Both temperatures result in higher molar fraction of DBP in distillate and lower DBP at residue. Equation 1 was proposed by the authors of [10] to transform the flash result into MD. The efficiency factor is multiplied with the molar fraction for DBP at distillate and DBP molar fraction at residue before mass balance equations are solved.

$$\eta = \frac{T_{flash} (K)}{T_{DISMOL} (K)} \quad (1)$$

$$\eta_{ASPEN PLUS} = \frac{336.26}{369} = 0.91$$

$$\eta_{ASPEN HYSYS} = \frac{336.66}{369} = 0.91$$

where η is the efficiency factor.

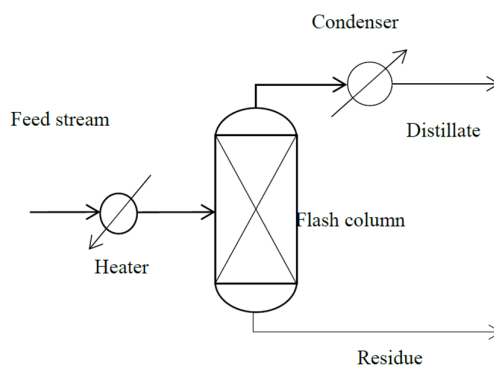
The results are summarized in Table 1. It is clear that the predictions of ASPEN HYSYS are close to that of ASPEN PLUS in terms of temperature and close to DISMOL in terms of Residue DBP molar fraction. In terms of distillation of DBP molar fraction, both ASPEN PLUS and ASPEN HYSYS predictions are within $\pm 2\%$ of that predicted by DISMOL. Thus, the developed flash process within ASPEN HYSYS can be applied to any MD process, such as the palm oil deodorization process considered in this work.

Table 1. Results of the DISMOL simulator, ASPEN PLUS and that developed in ASPEN HYSYS.

Parameters	DISMOL	ASPEN PLUS [10]	ASPEN HYSYS (This Work)
Operating temperature (K)	369	336	336
Distillation mass ratio	0.212	0.212	0.212
Distillation DBP molar fraction	0.775	0.790	0.793
Residue DBP molar fraction	0.429	0.409	0.420

3. Refined Palm Oil Deodorization Process Simulation by ASPEN HYSYS

The MD process model developed and validated in Section 2 is now used for the simulation of the deodorization of refined palm oil process in ASPEN HYSYS. Figure 3 shows the MD process for deodorization in refined palm oil. The operation is carried out at a high vacuum pressure between 5×10^{-4} and 8×10^{-4} kPa, at a temperature of 175 °C–180 °C and a feed flow rate between 250 and 2000 kg/h [11]. The vapor pressure estimations and the simulation of refined palm oil are discussed below.

**Figure 3.** Refined palm oil deodorization process.

3.1. Vapor Pressure Estimation

To design and simulate a molecular distillation, thermo-physical properties, vapor pressure of each component and the thermodynamic model are all required. This process used Redlich Kwong ASPEN (RK-Aspen) as a thermodynamic model or property method to calculate physical properties. The RK-Aspen is an equation of state model (EOS) that is good for vapor phase modeling with fewer binary parameters required and is consistent in critical region [12].

The feed stream of the process consists of five main components: tripalmitin triolein, oleic acid, tocopherol and beta-carotene. The mass fraction of each component is shown in Table 2. For a multicomponent system, it was not an easy task to calculate molar fraction by use of mass and component balances in an underdetermined situation. Consequently, thermodynamic properties and vapor pressure or pure component parameters for Antoine equations are required, and must be established.

Table 2. Composition of refined palm oil and its properties.

Components	Mass Fraction	MW	Formula	CAS No.
Tripalmitin	0.493682	807.320	C ₅₁ H ₉₈ O ₆	555-44-2
Triolein	0.470891	885.449	C ₅₇ H ₁₀₄ O ₆	122-32-7
Oleic acid	0.033899	282.467	C ₁₈ H ₃₄ O ₂	112-80-1
Tocopherol	0.000886	430.706	C ₂₉ H ₅₀ O ₂	59-02-9
Beta-carotene	0.000552	536.873	C ₄₀ H ₅₆	7235-40-7

The thermo-physical properties are introduced in the simulation in terms of physical properties such as boiling point (T_B), critical temperature (T_C), critical pressure (P_C), acentric factor (ω) and liquid molar volume (V_{l20}) for each component, and can be seen in Table A1 in the Appendix, as accomplished by Lim et al. [13]. Equation (2) refers to an extension of the Antoine equation from Lim et al.'s work, and its parameters are shown in Table 3. However, the equation available in ASPEN HYSYS is shown in Equation (3). Therefore, the parameters of the Antoine equation used in this study were obtained by minimizing the least square error of Equation (4) through Solver Add-in, in Microsoft Excel and Matlab optimization.

$$\ln P^{calc} = A_1 - B_1/T + C_1T + D_1 \cdot \ln T + E_1T^6 \quad (2)$$

$$\ln P^{exp} = A_2 + B_2/(T + C_2) + D_2 \cdot \ln T + E_2T^6 \quad (3)$$

where A, B, C, D and E are the Antoine Parameters. P is the vapor pressure in kPa, and T is temperature in K.

$$S = \sum_{i=1}^m [\ln P_i^{calc} - \ln P_i^{exp}]^2 \quad (4)$$

where S is sum of the squared error, m is the number of experimental data point within the temperature range of 373 K–503 K, P_i^{calc} is the calculated vapour pressure obtained from Lim et al.'s work [13] using Equation (2) and P_i^{exp} is the expected vapour pressure in Equation (3) (as available in ASPEN HYSYS). The pure component parameters for modified Antoine equation (Equation (3)) and coefficient of determination (R^2) of each component are summarized in Table 4. The coefficient of determination was calculated by regression data analysis in Microsoft Excel between the correlation of $\ln P^{calc}$ and $\ln P^{exp}$ as Equation (5).

$$R^2 = \frac{\text{Regression sum of square}}{\text{Total sum of square}} = \frac{\sum_{i=1}^m [\ln \hat{P}_i^{exp} - \ln \bar{P}_i^{exp}]^2}{\sum_{i=1}^m [\ln P_i^{exp} - \ln \bar{P}_i^{exp}]^2} \quad (5)$$

where $\ln P_i^{exp}$, $\ln \bar{P}_i^{exp}$ and $\ln \hat{P}_i^{exp}$ are the observed values of the dependent variable, mean or average and fitted values, respectively.

Table 3. Pure component parameters for Equation (2), reproduced with permission from [13]. Copyright Springer, 2003.

Component	Antoine Parameters				
	A_1	B_1	C_1	D_1	E_1
Tripalmitin	108,841	−4,098,952	19.96	−17,792	$−3.6 \times 10^{-15}$
Triolein	−514,215	19,737,838	−91.13	83,685	1.4×10^{-15}
Oleic acid	136.45	−19,702	−0.01	−14.87	7.2×10^{-19}
Tocopherol	−15.90	−5118	0.05	0	0.00
β-carotene	−91.32	−15.90	0.239	0	0.00

Table 4. Estimated pure component parameters for modified Antoine equation (Equation (3)).

Component	Antoine Parameters					R^2
	A_2	B_2	C_2	D_2	E_2	
Tripalmitin	1.509×10^5	1.196×10^5	$−0.074 \times 10^5$	$−0.21 \times 10^5$	0.00	0.99
Triolein	$−0.013 \times 10^7$	$−3.170 \times 10^7$	0.000	0.000	0.00	0.99
Oleic acid	519.688	−0.106	−399.010	−71.37	0.00	0.99
Tocopherol	−64.849	594.994	−219.253	13.052	0.00	0.99
β-carotene	24.079	−16,160	−100.623	5.191	0.00	0.99

3.2. Refined Palm Oil Deodorization Process Simulation and Validation

The main task of this part is to simulate, validate, and compare the performance of molecular distillation with 4 experiments reported in the patent of refining of edible oil rich in natural carotene and vitamin E [11]. The distillation mass ratio for the process was 0.036. The MD process was simulated, and prediction error of the simulations is shown in Table 5.

Table 5. Simulations results of refining of edible oil in study [11] and this work.

Condition	Distillation Mass Ratio	Patent Recovery		Simulation Recovery		Prediction Error
		kg/h	Percent (%)	kg/h	Percent (%)	(%)
Simulation 1	0.036	1.0395	95.98%	1.0351	98.96%	3.1%
Simulation 2	0.036	0.5449	98.73%	0.5467	99.03%	0.3%
Simulation 3	0.036	0.1249	98.03%	0.1266	99.29%	1.218%
Simulation 4	0.036	0.2969	97.38%	0.3258	99.25%	1.87%

The carotene recovery of the patent recorded in [11] and the current work is demonstrated in Figure 4. It can be clearly seen that the refined palm oil deodorization process simulation results show a very good agreement with the patent, with a prediction error of less than 3%.

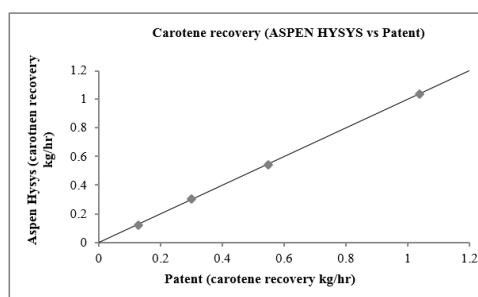


Figure 4. Carotene recovery of refining of edible oil in study [11] and this work.

4. RSM-Based Process Model

While we could use the ASPEN HYSYS based process model developed in Section 3 for further simulation and optimisation, here, we have decided to develop a Response Surface Methodology (RSM)-based process model and we resort to Design of Experiments (DoE). Like many authors [14,15] who have considered process simulator as an alternative to real process experiments and applied RSM on the simulated data in the past, we assume the ASPEN HYSYS based MD process described in Section 3 as the real process for the deodorization of refined palm oil.

The design of experiment (DoE) consists of three stages which are (i) screening methodology (preliminary research) to identify the vital factors, (ii) response surface methodology and (iii) model validation. The screening method is to detect factors that impact the process. In preliminary research for molecular distillation [6–9], it is found that temperatures at feed container, temperature at condenser and rotation speed of the design are the factors that had effects on the concentration of beta-carotene, tocopherol and free fatty acid. Therefore, these parameters are kept constant. Both temperatures at feed container and at condenser are fixed at 150 °C. In this work, the feed flow rate, column pressure and column temperature are manipulated for further investigation of the process.

RSM with Central Composite Design (CCD) is applied to develop, and obtain a quadratic model. The CCD consists of three portions which are the fraction of 2^k factorial design (level are coded as 1 and −1), $2k$ axial portion and the number of center point. In this case, the least number of 3 center points is used. Therefore, the design contained a total of 17 simulation runs according to Equation (6) [16]:

$$N = 2^k + 2k + n_0 \quad (6)$$

where N is the number total runs, k is independent variable, n_0 is number of center points.

The feed flow rate (x_1), distillation temperature (x_2), and pressure (x_3) were independent variables. These three variables are used and assumed to influence the responses of beta-carotene concentration (y_1), tocopherol concentration (y_2) at residue stream and free fatty acid (oleic acid) concentration (y_3) in the distillate stream.

In CCD, the axial value is set as 0.59. High value and low value are coded as 1 and -1 respectively while 0 was the center point code [17]. The coded values and its design range are shown in Tables 6 and 7 respectively. Those values are coded according to the following Equations (7)–(9) [17].

$$X_1 = \frac{x_1 - \bar{x}_1}{0.5 (x_{1H} - x_{1L})} = \frac{x_1 - 1500}{500} \quad (7)$$

$$X_2 = \frac{x_2 - \bar{x}_2}{0.5 (x_{2H} - x_{2L})} = \frac{x_2 - 150}{50} \quad (8)$$

$$X_3 = \frac{x_3 - \bar{x}_3}{0.5 (x_{3H} - x_{3L})} = \frac{x_3 - 5.05 \times 10^{-4}}{4.95 \times 10^{-4}} \quad (9)$$

where X_i and x_i are coded and actual values of variable i , respectively; and subscript i are 1 = feed flow rate, 2 = column temperature and 3 = column pressure, and H, L are highest and lowest values.

Table 6. Central composite circumscribed (Min and Max = Star Points) design with three independent variables.

Run	Coded Variables		
	X_1	X_2	X_3
1	0	0	−1
2	0	0	0
3	−1	0	0
4	0	0	0
5	0	1	0
6	−0.59	0.59	−0.59
7	0	0	0
8	0.59	−0.59	0.59
9	−0.59	−0.59	−0.59
10	0.59	0.59	0.59
11	0	−1	0
12	0.59	0.59	−0.59
13	−0.59	0.59	0.59
14	0.59	−0.59	−0.59
15	0	0	1
16	1	0	0
17	−0.59	−0.59	0.59

Table 7. Coded variables and design range.

Variables	Coded Variables and Design Range				
Feed flow rate (kg/h)	1000 (−1)	1203 (−0.59)	1500 (0)	1797 (0.59)	2000 (1)
Temperature (°C)	100 (−1)	120 (−0.59)	150 (0)	180 (0.59)	200 (1)
Pressure (kPa)	1.00×10^{-5} (−1)	2.11×10^{-4} (−0.59)	5.05×10^{-4} (0)	7.99×10^{-4} (0.59)	1.00×10^{-3} (1)

The regression analysis of the responses is fitted with non-linear second-order polynomial equation represented by Equation (10):

$$y = \beta_0 + \sum_{i=1}^3 \beta_i x_i + \sum_{i=1}^3 \beta_{ii} x_i^2 + \sum_{i=1}^3 \sum_{j=1}^3 \beta_{ij} x_i x_j \quad (10)$$

where y is the responses, β_0 is constant number, β_i , β_{ii} and β_{ij} are coefficients for the linear, quadratic and interaction, respectively.

Table 8 shows the experimental (simulated by MD process described in Section 3) results for 17 runs of independent variables with respect to responses: (y_1), (y_2) and (y_3). The regression coefficient value for linear, quadratic and interaction are shown in Table 9.

Table 8. Experimental design using Central Composite Design (CCD) of 17 runs.

Run	Input Variables			Composition Mass Fraction (Responses)		
	x_1 (kg/h)	x_2 (°C)	x_3 (10^{-4} kPa)	y_1 (10^{-4})	y_2 (10^{-4})	y_3
1	1500	150	0.10	0.28	0.54	0.09
2	1500	150	5.05	5.27	8.62	0.91
3	1000	150	5.05	5.27	8.62	0.91
4	1500	150	5.05	5.27	8.62	0.91
5	1500	200	5.05	7.27	9.63	0.08
6	1203	180	2.11	1.13	1.73	0.12
7	1500	150	5.05	5.27	8.62	0.91
8	1797	120	7.99	5.64	9.07	1.00
9	1203	120	2.11	5.57	9.04	0.99
10	1797	180	7.99	4.07	6.45	0.48
11	1500	100	5.05	5.57	8.95	1.00
12	1797	180	2.11	1.13	1.73	0.12
13	1203	180	7.99	4.07	6.45	0.48
14	1797	120	2.11	5.57	9.04	0.99
15	1500	150	1.00	5.48	8.89	0.96
16	2000	150	5.05	5.27	8.62	0.91
17	1203	120	7.99	5.64	9.07	1.00

The effect of each independent variable on the responses according to 17 runs is described below.

Table 9. Estimated regression coefficient for refined palm oil.

Term	Coefficient	Coefficient	Coefficient
Constant	5.25×10^{-4}	8.60×10^{-4}	9.15×10^{-1}
x_1	1.35×10^{-20}	3.49×10^{-20}	-1.27×10^{-18}
x_2	-2.49×10^{-4}	-4.12×10^{-4}	-5.34×10^{-1}
x_3	1.83×10^{-4}	2.92×10^{-4}	2.69×10^{-1}
x_1x_1	2.42×10^{-5}	3.54×10^{-5}	-1.63×10^{-3}
x_2x_2	-1.88×10^{-4}	-3.31×10^{-4}	-3.74×10^{-1}
x_3x_3	-2.15×10^{-4}	-3.56×10^{-4}	-3.91×10^{-1}
x_1x_2	6.88×10^{-21}	-1.38×10^{-20}	2.82×10^{-17}
x_1x_3	-1.38×10^{-20}	9.01×10^{-21}	2.73×10^{-17}
x_2x_3	2.07×10^{-4}	3.38×10^{-4}	2.50×10^{-1}

4.1. The Effect of Feed Flow Rate on Responses

The results of feed flow rate on the responses of beta-carotene (y_1), tocopherol (y_2) and FFA (y_3) are investigated at a temperature of 150 °C and pressure of 5.05×10^{-4} kPa (run No. 2 and 3). Decreasing the feed flow rate from 1500 to 1000 kg/h at constant temperature and pressure does not make any changes to the responses. The contour plots and response surface curves in Figures 5–7, reveal that the feed flow rate does not show significant deviation on responses.

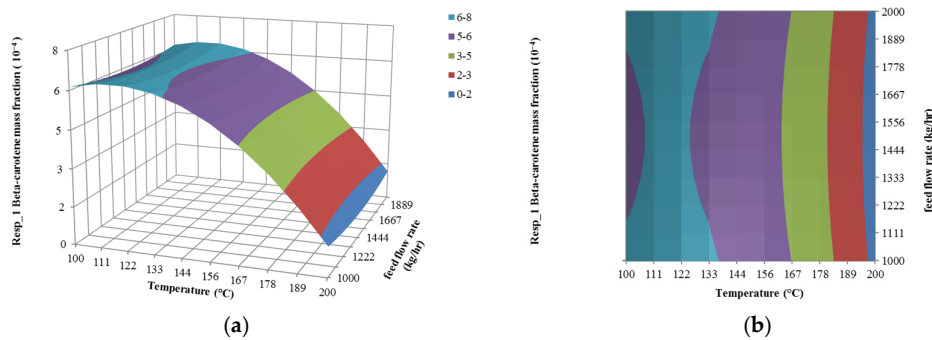


Figure 5. Response surface curve (a) and contour plot (b) of beta-carotene concentration as a function of temperature and feed flow rate.

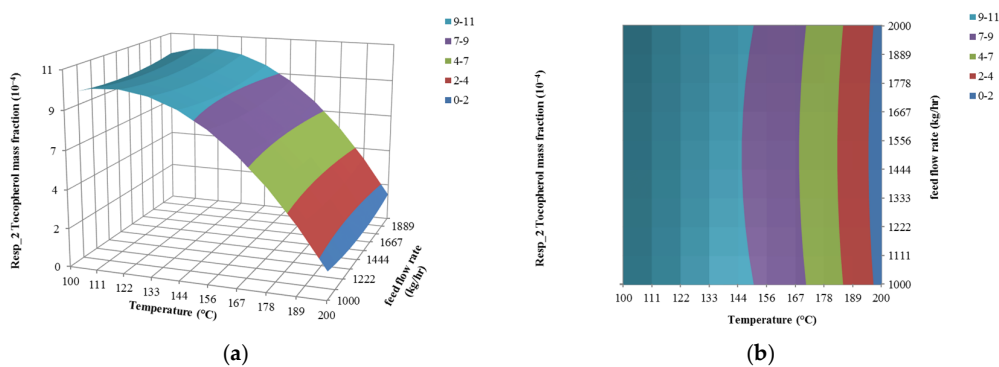


Figure 6. Response surface curve (a) and contour plot (b) of tocopherol concentration as a function of temperature and feed flow.

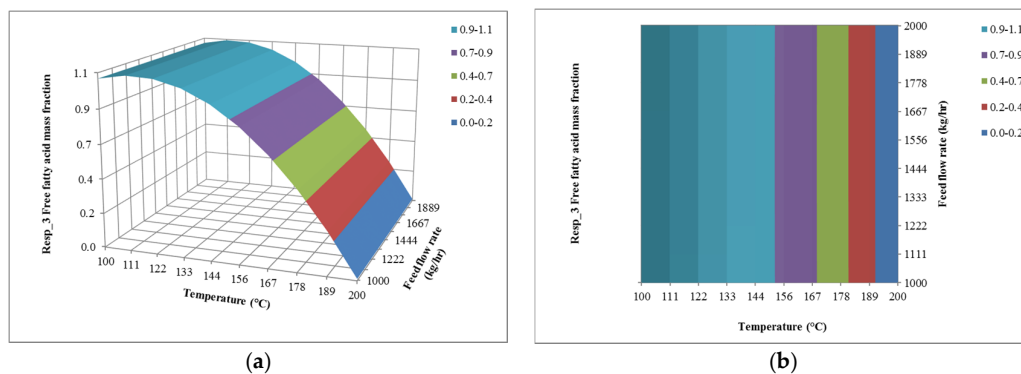


Figure 7. Response surface curve (a) and contour plot (b) of FFA concentration as a function of temperature and feed flow.

4.2. The Effect of Temperature on Responses

Concentration of beta-carotene, tocopherol and FFA as a function of temperature are investigated at constant feed flow rate and pressure at 1500 kg/h and 5.05×10^{-4} kPa respectively (run no. 4 and 5). In Figures 8–10, the temperature shows significant deviation in the responses of beta-carotene (y_1), tocopherol (y_2) and FFA (y_3). It can be clearly seen that, the concentrations of the responses decrease with increasing the distilling temperature. According to the Clausius Clapeyron relation, the vapor pressure of substance increases non-linearly with temperature. Therefore, increasing temperature (Equation (11)) will increase mean free path which will lengthen the average distance of traveling molecule reaching the condensation board. The longer the distance of molecule travels the higher the

rate of vaporization of molecule. As a result, low concentration of beta-carotene and tocopherol are found in the residue and low concentration of free fatty acid is found in the distillate.

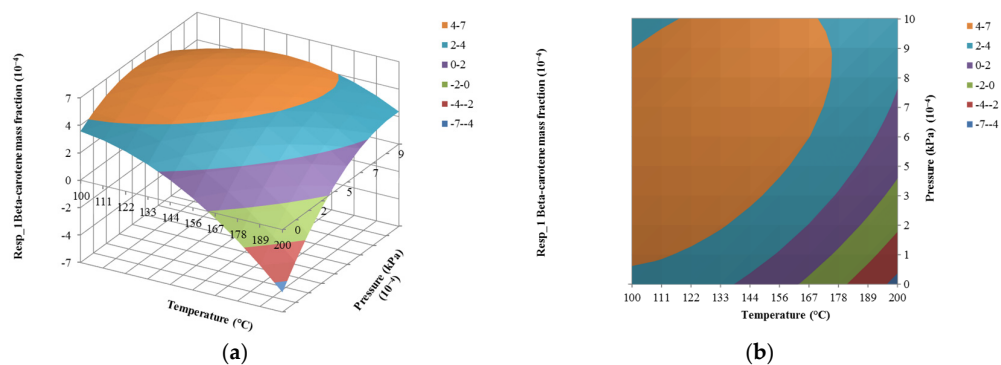


Figure 8. Response surface curve (a) and contour plots (b) of beta-carotene concentration as a function of temperature and pressure.

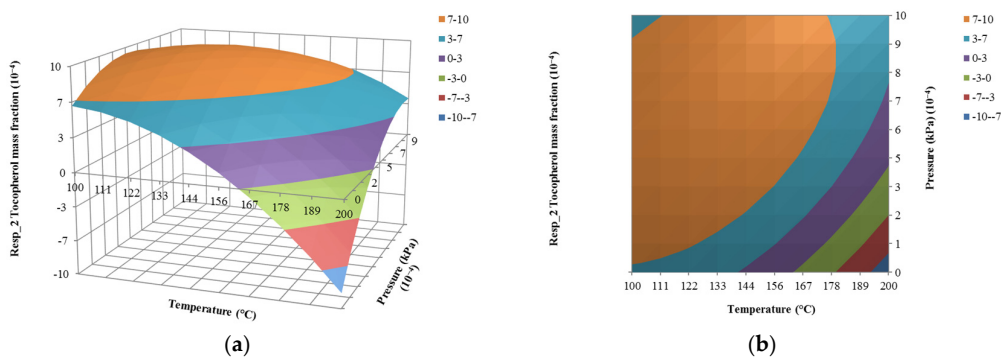


Figure 9. Response surface curve (a) and contour plot (b) of tocopherol concentration as a function of temperature and pressure.

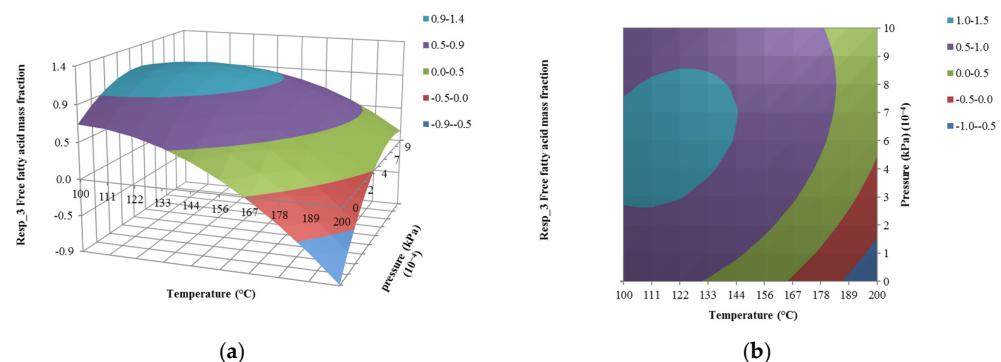


Figure 10. Response surface curve (a) and contour plot (b) of free fatty acid (FFA) concentration as a function of temperature and pressure.

4.3. The Effect of Pressure on Responses

The effect of pressure on responses (composition of beta-carotene, tocopherol and FFA) is investigated at feed flow 1500 kg/h and at temperature of 150°C (run no. 1, 2, 7 and 15). The responses are found to increase with the increase of pressure, as can be seen in Figures 8–10. In agreement with the theory of mean free path for molecular distillation as shown in Equation (11), increasing the pressure will reduce the mean free path, which shortens the average distance of molecules reaching the

condensation board. The shorter the average distance of traveling molecule the lesser the vaporization of molecule. Consequently, high concentration of beta-carotene and tocopherol are achieved at residue stream which consequently increase the free fatty acid concentration at the distillate.

$$\lambda = \frac{RT}{\sqrt{2}\pi d^2 N_A P} \quad (11)$$

where λ is the mean free path, R is gas constant, d is molecular diameter N_A is Avogadro's number and P is the pressure.

The independent variables and responses are fitted by the following second order polynomial Equations (12)–(14) which show complex relationships between the independent variables and the responses. In addition, term constants of x_1 , x_1x_2 , and x_1x_3 are not considered in this case due to the insignificant effect to the responses.

$$y_1 = 5.25 \times 10^{-4} - 2.49 \times 10^{-4}x_2 + 1.83 \times 10^{-4}x_3 + 2.42 \times 10^{-5}x_1^2 - 1.88 \times 10^{-4}x_2^2 - 2.15 \times 10^{-4}x_3^2 + 2.07 \times 10^{-4}x_2x_3 \quad (12)$$

$$y_2 = 8.60 \times 10^{-4} - 4.12 \times 10^{-4}x_2 + 2.92 \times 10^{-4}x_3 + 3.54 \times 10^{-5}x_1^2 - 3.31 \times 10^{-4}x_2^2 - 3.56 \times 10^{-4}x_3^2 + 3.38 \times 10^{-4}x_2x_3 \quad (13)$$

$$y_3 = 9.15 \times 10^{-1} - 5.34 \times 10^{-1}x_2 + 2.69 \times 10^{-1}x_3 - 1.63 \times 10^{-3}x_1^2 - 3.74 \times 10^{-1}x_2^2 - 3.91 \times 10^{-1}x_3^2 + 2.50 \times 10^{-1}x_2x_3 \quad (14)$$

The R^2 value of responses, concentration of beta-carotene, tocopherol and FFA are 0.959, 0.961 and 0.951 respectively, show a very good fit. The nonlinear Equations (12)–(14) now represent the MD process model which will be used for optimizing the process in the next section.

It is observed that the response surface curves of beta-carotene, tocopherol and FFA concentration display a similar relationship with respect to independent variables. The concavity of the curves shows the optimum point of each of the responses. However, those concavities are not high enough to indicate the visually maximum point of responses.

5. Optimization of MD for Refined Palm Oil Process

In this section the aim is to find the optimum operating parameters that will maximize the concentration of beta-carotene, tocopherol at the residue and concentration of FFA at the distillate stream. The mathematical model (Equations (12)–(14)) and the objective function have been written in Equation (15). This work is more concerned with the enhancement of concentration of beta-carotene and tocopherol as 70%, than it is with reducing the concentration of free fatty acid. Therefore, in the objective function, different weighting was applied by a factor of 0.7 in y_1 , y_2 and 0.3 for y_3 . The optimization variables are feed flow rate, temperature and pressure. Lower and upper bounds for variables are specified between a valid lower and upper bound. The actual (re-scaled) upper bound and lower bound is shown in the Table 10.

$$\text{Maximize: } f(x) = 0.7(y_1 + y_2) + 0.3y_3 \quad (15)$$

Table 10. Upper bound and lower bound for independent variables.

Variable Description	Low Bound	High Bound
Inlet Mass flow rate (kg/h)	1000	2000
Temperature (°C)	100	200
Pressure (kPa)	0.001	0.00001

Subject to: $h(x) = 1000 \leq x_1 \leq 2000$, $100 \leq x_2 \leq 200$, $0.00001 \leq x_3 \leq 0.001$, $0 \leq y_1 \leq 1$, $0 \leq y_2 \leq 1$, $0 \leq y_3 \leq 1$.

Solver in Microsoft Excel is an efficient tool to solve both equality and inequality constrained non-linear optimization problem [18]. An Excel worksheet for optimization is prepared as shown in

Figure A1. The objective function is set to target cell for maximization by changing the independent variables (refer to Figure A2). Initial value for feed flow rate, temperature and pressure were set as 1500 kg/h, 150 °C and 0.00055 kPa, respectively. The solution method used for this work is evolutionary; it is for solving a non-smooth non-linear equation. The optimum results of x_1 , x_2 and x_3 were found to be 1291 kg/h, 147 °C and 0.0007 kPa, respectively, and the corresponding responses of y_1 , y_2 and y_3 were 0.000575, 0.000937 and 0.999840, respectively.

Lastly, model validation is performed to ensure that data inserted into simulation satisfied the prediction. ASPEN HYSYS is simulated using the optimum operating conditions. The responses are shown in Table 11 and regression statistic of model and simulation is shown in Table 12. Clearly, the model equations developed from RSM can be used for predicting responses of the deodorization process.

Table 11. Predicted result from the Response Surface Methodology (RSM) model and ASPEN HYSYS Simulation.

Components	Responses Result from RSM Model	Responses Result from ASPEN HYSYS Simulation
Beta-carotene	0.000554	0.000545
Tocopherol	0.000896	0.000890
FFA	0.999000	0.953000

Table 12. The regression statistics of model and simulation.

Parameters	Regression Statistics
Multiple R	1
R Square	1
Adjusted R Square	1
Standard Error	3.18×10^{-6}
Observations	3

6. Conclusions

Simulation and optimization of the refined palm oil process has been considered in this work. A single flash vessel model is developed in ASPEN HYSYS to represent Molecular Distillation (MD) of the refined palm oil process, which has been validated with experimental results from the literature with prediction efficiency errors of less than 3%. Response surface methodology with central composite design was then applied to design of experiments with the validated ASPEN HYSYS model to investigate the effects of feed flow rate, temperature and pressure on concentration of beta-carotene, tocopherol and free fatty acid (FFA) in the MD. The results show that response surface curves of beta-carotene, tocopherol and FFA displayed a similar relationship with respect to temperature and pressure. The result suggested that temperature and pressure and their interaction significantly influences the responses of beta-carotene, tocopherol and FFA, while feed flow rate and their interaction less significantly affected by the responses of beta-carotene, tocopherol and FFA. Finally, the process optimization through Excel solver was carried out using RSM equations, and the optimum operating parameters of MD for refined palm oil process were obtained. These parameters are feasibly suitable for refined palm oil in industrial manufacturing.

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Author Contributions: This research was carried out in collaboration of all authors. Noree Tehlah performed the simulation and wrote the manuscript. Pornsiri Kaewpradit and Iqbal M. Muftaba supervised statistical analysis, analysed results, oversaw and approved the final manuscript.

Conflicts of Interest: The authors declare no conflict of interest.

Appendix

Table A1. Physical properties of pure components in palm oil, reproduced with permission from [13]. Copyright Springer, 2003.

Component	T_B (K)	T_C (K)	P_C (kPa)	ω	V_{120} (m ³ /kmol)
Tripalmitin	864.21	947.10	396.82	1.6500	0.8906
Triolein	879.92	954.10	360.15	1.8004	0.9717
Oleic acid	646.52	813.56	1250.2	0.8104	0.3172
Tocopherol	794.52	936.93	838.45	1.1946	0.4533
Beta-carotene	908.58	1031.1	678.41	1.6255	0.5348

	A	B	C	D	E
1					
2	Coefficient value given by RSM without consider P value				
3		Response 1 coefficient	Response 2 coefficient	Response 3 coefficient	
4	β_0	0.000525	0.000860	0.915000	
5	β_1	0.000000	0.000000	0.000000	
6	β_2	-0.000249	-0.000412	-0.534000	
7	β_3	0.000183	0.000292	0.269000	
8	β_4	0.000024	0.000035	-0.001630	
9	β_5	-0.000188	-0.000331	-0.374000	
10	β_6	-0.000215	-0.000356	-0.391000	
11	β_7	0.000000	0.000000	0.000000	
12	β_8	0.000000	0.000000	0.000000	
13	β_9	0.000207	0.000338	0.250000	
14					
15					
16					
17					
18					
19					
20					
21	feed flow rate kg/hr				
22	1291				
23					
24					
25					
26					
27					
28					
29					
30					
31					
32					
33					
34					
35					
36					
37	Term	Feed flow rate kg/hr	Temperature °C	Pressure kPa	
38	Data Minimum	1000	100	0.000010	
39	Data Average	1500	150	0.000550	
40	Data Maximum	2000	200	0.001000	
41	Term	response 1(Y_1)	response 2(Y_2)	response 3(Y_3)	
42	Data Minimum	0	0	0	
43	Data Average	0.5	0.5	0.5	
44	Data Maximum	1	1	1	

Pressure kPa	0.0007
Temperature °C	147

Non-linear equation for Y_1
 $=B_4 + B_5 \times A_{23} + B_6 \times C_{26} + B_7 \times C_{20} + B_8 \times A_{23} \times A_{23} + B_9 \times C_{26} \times C_{26} + B_{10} \times C_{20} \times C_{20} + B_{11} \times A_{23} \times C_{26} + B_{12} \times A_{23} \times C_{20} + B_{13} \times C_{26} \times C_{20}$

Response 1 (Y_1)	0.0005753
Response 2 (Y_2)	0.0009372
Response 3 (Y_3)	0.9999840
Objective function	1.0014965

$0.7(Y_1 + Y_2) + 0.3(Y_3)$

Figure A1. The solver Excel spread sheet.

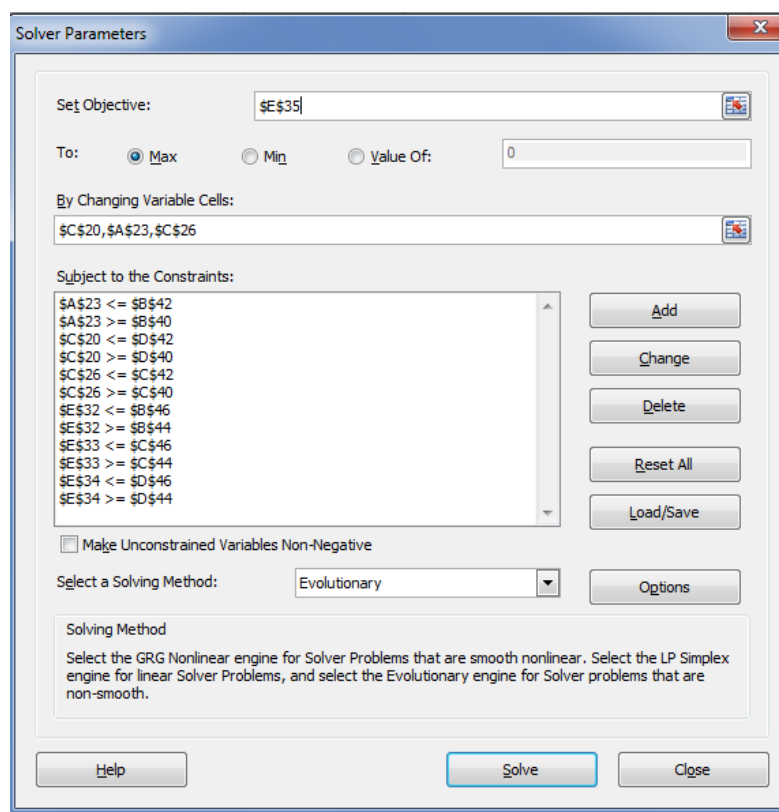


Figure A2. The solver parameters.

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